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## Tentative Identification of the Reactive Species in the Reaction of Cp<sub>2</sub>TiCl<sub>2</sub> with Salts of Diacids

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#### ABSTRACT

The tentative identification of the reactive species in the condensation of  $Cp_2TiCl_2$  with salts of diacids to form titanium polyesters is made. The reactive species are believed to be the same for both aqueous solution and interfacial systems, i.e.,  $R-CO_2^-$  and  $Cp_2Ti^{2+}$  with reaction occurring in the aqueous phase. The condensation of  $Cp_2TiCl_2$  with disodium terephthalate in interfacial systems occurs via a pseudo-first-order reaction:

Rate =  $k[Cp_2TiCl_2]$ 

The rate-determining step(s) is believed to be diffusion of  $CP_2 TiCl_2$  into the aqueous layer and/or hydrolysis of  $Cp_2 TiCl_2$ .

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#### INTRODUCTION

We have previously reported the initial synthesis of titanium polyesters of Form I utilizing both interfacial and solution techniques [1, 2]. More recently we reported the thermal stability and "anomalous fiber formation" for some of the products [3]. We now report on several reaction variables associated with the synthesis of the polyesters. Reasons for desiring the synthesis of such products are cited elsewhere as is previous work involving titanium esters [1, 2].

$$Cp_{2}TiCl_{2} + {}^{\Theta}O - C - R - C - O^{\Theta} \rightarrow \begin{bmatrix} Cp & O & O \\ | & || & || \\ Ti - O - C - R - C - O \\ | & Cp \end{bmatrix}$$

$$I$$

#### EXPERIMENTAL

The following reagents were used without further purification: dicyclopentadienyltitanium dichloride (Alfa Inorganics, Inc., Beverly, Massachusetts); all of the diacids were obtained from Aldrich Chemical Co., Milwaukee, Wisconsin.

Polymerization procedures are given elsewhere [1, 2]. Briefly, solutions of  $Cp_2TiCl_2$  are added to stirred solutions containing salts of diacids. For interfacial systems,  $Cp_2TiCl_2$  is contained in an organic solvent, whereas for aqueous solution systems it is contained in water.

Light scattering, elemental analysis, IR spectroscopy, viscometry, and solution techniques are the same as those employed previously [1, 2]. Elemental analysis and IR spectra are in agreement with a product of repeating unit 1. Many of the products are insoluble in all attempted solvents. Viscosity and/or weight-average molecular weight results are reported for those which are soluble.

Condensations were carried out using a blender whose 'no-load'' speed was standardized using a strobotac, type 1531-A (General Radio Company, Concord, Maryland). The blender was connected to a Powerstat, Type 116 (Superior Electric Co., Bristol, Connecticut) and the speed measured as a function of powerstat reading.

#### **RESULTS AND DISCUSSION**

The purpose of this research was to tentatively identify the reactive species and site for the interfacial systems, and to evaluate particular reaction parameters for which other similar systems have shown dependencies.

Results aimed at determining the kinetic behavior, active species, and site(s) of polycondensation for interfacial systems have been quite limited mainly due to 1) rapidity of reactions, many being completed in less than 60 sec; 2) complexity of reaction, reaction pathways, and reaction species; 3) complexity of reaction system, rapidly stirred and heterophasic; 4) lack of prior similar and/or credulous research in analogous organometallic condensations; and 5) many of the organometallic products are insoluble in all solvents precluding determinations requiring solution of the products [4]. The present system suffers to some degree from all of these problems, necessitating the speculative nature of the results.

The exact form of the aqueous solubilized Cp<sub>2</sub> TiCl<sub>2</sub> is unknown. Various structures have been suggested which include  $Cp_2TiOH^+$  and Cp<sub>2</sub>Ti<sup>2+</sup> [5-7]. Aqueous solutions probably contain several species with the relative abundance varying with pH. Aqueous solutions of Cp, TiCl, are acidic, exhibiting pH's in the range of 1 to 2. This is indicative of hydrolysis of Cp<sub>2</sub>TiCl<sub>2</sub> which favors the presence of species such as  $Cp_2 TiOH^+$ . A 0.08 <u>M</u> solution of  $Cp_2 TiCl_2$  gives a pH of 1.7 corresponding to a  $Cp_2 Ti^{2+}:Cp_2 TiOH^+$  of 3:1 assuming these to be the most prevalent species. At high pH's, insoluble  $Cp_2 Ti(OH)_2$ is formed. Aqueous solutions of  $Cp_2TiCl_2$  can be evaporated to dryness to give Cp, TiCl, back again quantatively. Thus solubilization of Cp, TiCl, to form various ions is reversible. Other characteristics of aqueous solutions of  $Cp_2 TiCl_2$  have been reported elsewhere [1, 2]. For simplicity, Cp, TiCl, solubilized in water will be designated as  $Cp_2Ti^{2+}$ . The active form of the salt is presumably the anion,  $RCO_2$ for aqueous solution systems.

Evidence as to the active species was sought by comparing the relative reactivity trends for interfacial and aqueous solution systems as a function of substituted terephthalic acid. If the reactive species is the same for both systems, then the orders and/or general dependencies should be the same for both systems, the only difference being the presence of an organic layer which supplies a constant supply of  $Cp_2TiCl_2$ , i.e., the active titanium species in both systems is the  $Cp_2Ti^{2+}$  formed in the interfacial systems via migration from the organic layer to the aqueous layer and the active acid form is the salt,  $RCO_2^-$ , with the reaction occurring in the aqueous phase to allow

hydrolysis of  $Cp_2 TiCl_2$ . All systems were run to completion, i.e., 1 min stirring time is greater than the reaction time; thus yield is a measure of the overall efficiency of polyester formation.

The trends are similar and follow a trend tetramethylterephthalate > dimethylterephthalate > terephthalate > bromoterephthalate > dichloroterephthalate > nitroterephthalate which is the trend of decreasing basicity of the  $RCO_2^{-}$  [8]. This is consistent with reaction occurring via a simple addition pathway and also with reaction occurring in the aqueous phase for the interfacial systems. The latter is not unexpected since the solubility of the salt in the organic phase should be quite low.

A similar comparative study has been carried out between the reaction of  $Cp_2 TiCl_2$  with substituted hydroquinones to form polyethers [9]. For these systems yield trends were dissimilar with steric hindrance being a critical factor for interfacial systems, which was consistent with a more sterically dependent bimolecular reaction between R-OH and  $Cp_2 TiCl_2$  occurring in interfacial systems. Other evidence was consistent with polyesterification occurring via different pathways for interfacial and solution systems with reaction occurring in the organic layer, near the interface for interfacial systems.

Reactions in aqueous solution systems are too rapid to follow using conventional techniques. Reaction in interfacial systems is somewhat slower, and a kinetic study was attempted using terephthatic acid and  $Cp_2 TiCl_2$ . Addition of the reactants to one another was rapid and controlled such that addition of 100 ml of solution required less than 5 sec. Reaction time was begun after addition of the two phases. Treatment of the data is open to discussion. Concentrations are calculated based on the amount of reactant present compared to the total volume of both phases. Reaction rates and concentrations of reactants are based on the amount of polymer formed. This is believed to be valid since an investigation of the species present does not indicate the presence of other nonpolymer using products.

The data were treated in the usual manner and yield linear plots of  $\log [Cp_2TiCl_2]_{initial}/[CpTiCl_2]$  as a function of time and rate as a function of reactant concentration, i.e., first-order relationships (Fig. 1). Further work was done. By varying the amounts of reactants, it was found that the rate is primarily dependent on the concentration of the Cp\_TiCl\_ but not greatly affected by the concentration of the disodium terephthalate (range tested = 0.015 to 0.045 <u>M</u>), being in agreement with the expression

Rate =  $k[Cp_2TiCl_2]$ 

The reaction is believed to be pseudo-first-order since 1) it is apparent that yield is dependent on the nature of the diacid (cf., for instance, Table 1), and 2) the plots of rate vs  $[Cp_2TiCl_2]$  and log

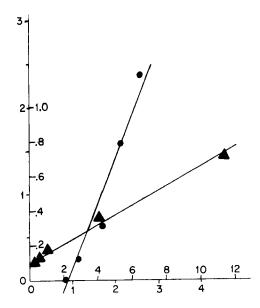


FIG. 1. Kinetic data for the condensation of  $Cp_2TiCl_2$  (0.00125 mole) in 30 ml chloroform and disodium terephthalate (made from the addition of 0.00250 mole of sodium hydroxide to 0.00125 mole of terephthalate acid) in 10 ml of water at  $27^{\circ}C$  with a stirring rate of 17,500 rpm plotted for first-order kinetic relationships. Outside ordinate values: Rate [moles/(liter)(sec) × 10<sup>-4</sup>] (•). Outside abscissa values: [ $Cp_2TiCl_2$ ] × 10<sup>2</sup> (•). Inside abscissa values: [ $Cp_2TiCl_2$ ] o

 $\log \frac{\left[ Cp_2 TiCl_2 \right]_0}{\left[ Cp_2 TiCl_2 \right]_{time}}$  ( ). Inside abscissa values: Reaction time

time (min) (  $\blacktriangle$  ).

 $[Cp_2 TiCl_2]_{initial}/[Cp_2 TiCl_2]$  vs time do not pass through the ordinate as true first-order plots should.

Product molecular weight appears to be constant with reaction time for this system with an average limiting viscosity number of 0.15 dl/gand a weight-average molecular weight of  $3 \times 10^5$  via light-scattering photometry. This is consistent with a chain-type mechanism proposed for many interfacial condensations (for instance, Refs. 4 and 10).

A similar kinetic behavior was reported for the interfacial condensation of  $Cp_2 ZrCl_2$  with the disodium salt of 1,1'-ferrocene dicarboxylic acid [11]. To further evaluate the kinetic behavior, the

| Acid                         | Yield (%)       |                  |
|------------------------------|-----------------|------------------|
|                              | Interfacial     | Aqueous solution |
| Tetramethylterephthalic acid | 76              | 59               |
| Dimethylterephthalic acid    | 65              | 47               |
| Terephthalic acid            | 55 <sup>b</sup> | 48 <sup>c</sup>  |
| Bromoterephthalic acid       | 33              | 43               |
| Dichloroterephthalic acid    | 30              | 32               |
| Nitroterephthalic acid       | 28              | 27               |

TABLE 1. Yield as a Function of Substituted Terephthalic Acid<sup>a</sup>

<sup>a</sup>Reaction conditions: For interfacial systems the sodium salts of dicarboxylic acids (prepared from addition of 0.00125 mole of diacid to 0.00375 mole of NaOH) in 30 ml of  $H_2O$  were added to rapidly stirred (rpm = 21,500) solutions of  $Cp_2 TiCl_2$  (0.00125 mole) in 30 ml of CHCl<sub>3</sub> at 27°C for 1 min stirring time. Aqueous solution systems were prepared in the same way except  $Cp_2 TiCl_2$  was contained in 30 ml of  $H_2O$ .

<sup>b</sup>LVN = 0.15/dl/g and  $\overline{M}_{W}$  via light scattering of  $3 \times 10^{5}$ , both in 2-chloroethanol at  $30^{\circ}$ C.

 $^{\rm C}$ LVN = 0.08 dl/g in 2-chloroethanol at 30°C.

system was studied as a function of stirring rate. Yield remains essentially constant throughout the stirring range of 10,100 to 24,400 rpm. According to Smirhova [12], a constancy of yield as stirring rate is varied means the reaction is "kinetically controlled."

The Cp  $_2$ TiCl $_2$  possesses two color sites, the yellow Cp-Ti and the red Ti-Cl [1, 2]. Interfacial reactions progress through a series of color changes from red to pink to yellow. The appearance of the yellow color was always found experimentally to coincide with the completion of the reaction and can be utilized as a crude measure of the rates of reaction. The time required for onset of the yellow coloration is listed in Tables 2 and 3 as the "color change time." Color change time decreases (i.e., reaction rate increases) with an increase in stirring rate (Table 2). Such reactions should then be viewed as diffusion controlled (i.e., differences in yield and/or rate are brought about by differences in diffusion, assuming that increased stirring rates effect only increases in interfacial surface area [12, 13]) and not as "kinetically controlled." (The systems utilized in the kinetic studies did not exhibit the onset of yellow coloration.)

| Stirring rate<br>(rpm) | Yield<br>(%) | Color change time <sup>b</sup><br>(sec) |
|------------------------|--------------|---|
| 10,000                 | 50           | 60                                      |
| 15,200                 | 64           | 55                                      |
| 18,100                 | 54           | 45                                      |
| 21,500                 | 55           | 25                                      |
| 22,400                 | 55           | 25                                      |
| 24,400                 | 55           | 20                                      |

TABLE 2. Yield as a Function of Stirring Rate for Interfacial Systems<sup>a</sup>

<sup>a</sup>Reaction conditions the same as given in Table 1 for terephthalic acid except for stirring rate.

<sup>b</sup>Reported to the nearest 5 sec.

| CHCl <sub>3</sub> volume | Yield (%) | Color change time <sup>b</sup><br>(sec) |
|--------------------------|-----------|---|
| 30                       | 55        | 25                                      |
| 60                       | 52        | 35                                      |
| 120                      | 5         | 60                                      |
| 150                      | 3         | 60                                      |

### **TABLE 3.** Yield as a Function of Organic Volume<sup>a</sup>

<sup>a</sup>Reaction conditions the same as given in Table 1 for terephthalic acid except for volume of  $CHCl_3$ .

bReported to the nearest 5 sec.

It is currently believed that the rate-determining reaction is the diffusion of the  $Cp_2 TiCl_2$  through the interface into the aqueous layer and/or the hydrolysis of the  $Cp_2 TiCl_2$ , either or both responsible for 1) the pseudo-first-order rate dependence on  $Cp_2 TiCl_2$  and 2) the color changes observed as a function of stirring rate.

The importance of diffusion and/or hydrolysis of  $Cp_2 TiCl_2$  is further borne out by the dependence of yield and "color change time" on the volume of the organic phase with color change time becoming less and yield becoming greater as chloroform volume is decreased (Table 3).

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